

## Lecture 8 Flow around a cylinder

Assuming irrotational flow  $\nabla \times \mathbf{v} = 0$

So using potential

$$\mathbf{v} = \nabla \phi$$

~~In addition assume~~

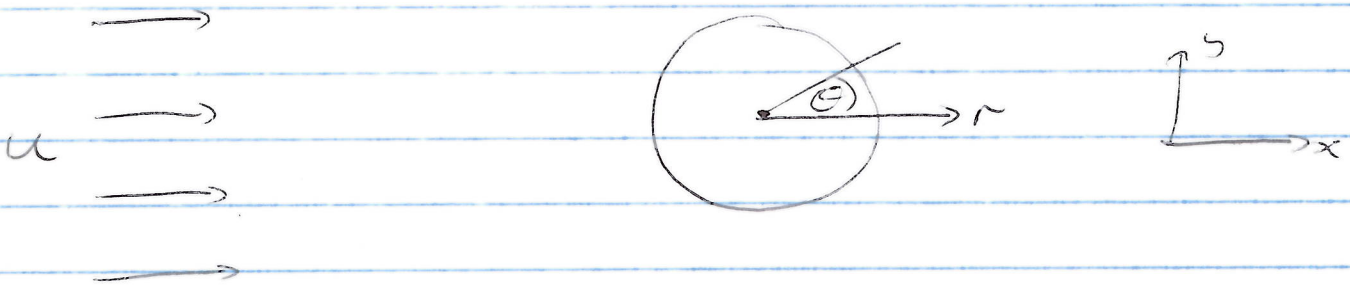
Since flow is incompressible  $\nabla \cdot \mathbf{v} = 0$

so

$$\nabla^2 \phi = 0$$

(Laplace's equation)

Consider a cylinder in a uniform flow



In polar coordinates

$$\nabla^2 \phi = \frac{\partial^2 \phi}{\partial r^2} + \frac{1}{r} \frac{\partial \phi}{\partial r} + \frac{1}{r^2} \frac{\partial^2 \phi}{\partial \theta^2} = 0$$

Boundary conditions

(1) No flow through surface so

$$\frac{\partial \phi}{\partial r} = 0 \text{ at } r = a$$

(2) Velocity  $\rightarrow u$  in  $x$  direction as  $r \rightarrow \pm \infty$

$$\phi \rightarrow ur \cos \theta \text{ as } r \rightarrow \pm \infty$$



8.2

Look for  $\phi = \phi_r(r) \phi_\theta(\theta)$

$$\phi_\theta \left( \frac{\partial^2 \phi_r}{\partial r^2} + \frac{1}{r} \frac{\partial \phi_r}{\partial r} \right) + \phi_r \frac{1}{r^2} \frac{\partial^2 \phi_\theta}{\partial \theta^2} = 0$$

$$\frac{r^2}{\phi_r} \left( \frac{\partial^2 \phi_r}{\partial r^2} + \frac{1}{r} \frac{\partial \phi_r}{\partial r} \right) = - \frac{1}{\phi_\theta} \frac{\partial^2 \phi_\theta}{\partial \theta^2} = \lambda$$

Must be a constant since LHS only f(r) and RHS f(\theta)

\(\Rightarrow\) \(\theta\) dependent

$$\frac{\partial^2 \phi_\theta}{\partial \theta^2} = -\lambda \phi_\theta \quad \phi_\theta = A \sin(\lambda^{1/2} \theta) + B \cos(\lambda^{1/2} \theta)$$

To match boundary at  $r = \infty$ , only  $\cos \theta$  term,  $\lambda = 1$

$$\Rightarrow \phi_\theta = B \cos \theta$$

r dependent

$$r^2 \frac{\partial^2 \phi_r}{\partial r^2} + r \frac{\partial \phi_r}{\partial r} - \phi_r = 0$$

try  $\phi_r = A r^n$

$$r^2 A n(n-1) r^{n-2} + r n A r^{n-1} - A r^n = 0$$

$$\Rightarrow n(n-1) + n - 1 = 0$$

$$\underline{n=1 \text{ or } -1}$$

$$\Rightarrow \phi_r = A r + \frac{C}{r}$$

As  $r \rightarrow \infty$   $\phi_r \rightarrow A r = u r \Rightarrow \underline{A = u}$

at  $r = a$   $\frac{\partial \phi_r}{\partial r} = 0 \Rightarrow A - \frac{C}{a^2} = 0 \Rightarrow \underline{\underline{C = a^2 u}}$

So the solution is

$$\underline{\phi = u \left( r + \frac{a^2}{r} \right) \cos \theta}$$

However we can add to this

① a constant, but this has no effect ( $v = \nabla \phi$ )

② a linear function of  $\theta$

$$\phi = \frac{\Gamma \theta}{2\pi} \quad \Gamma = \text{circulation}$$

$$\boxed{\phi = u \left( r + \frac{a^2}{r} \right) \cos \theta + \frac{\Gamma \theta}{2\pi}}$$

not unique, requires knowledge of circulation either from

① Ad-hoc assumption, used subtly

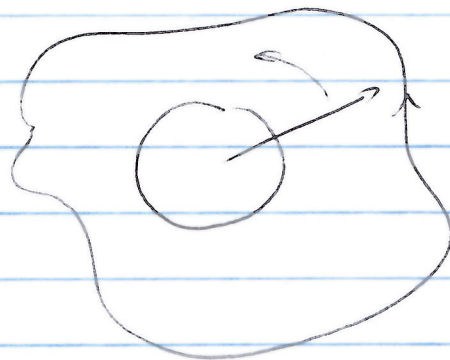
② viscous boundary effects not included in irrotational flow theory.

What effect does this circulation have?

→ will show that this is the origin of lift, via the Kutta-Joukowski theory.

Why is  $\Gamma$  circulation?

$$\Gamma = \oint_C \underline{v} \cdot d\underline{c} = \underbrace{\oint_C \nabla \phi \cdot d\underline{c}}_{\text{change in } \phi \text{ after one circuit}}$$



$\Theta$  changes by  $2\pi$

$\phi$  changes by  $\Gamma$



8.3 Apply Bernoulli's theorem to the flow around a cylinder.

$$p + \frac{1}{2} \rho u^2 = \text{const} \quad \text{on cylinder surface}$$

since it's a streamline

$$u_r = 0 \quad \text{at } r = a$$

$$u_\theta = \frac{1}{r} \frac{\partial \phi}{\partial \theta} = -u \left( 1 + \frac{a^2}{r^2} \right) \sin \theta + \frac{\Gamma}{2\pi r}$$

Here at  $r = a$

$$= -2u \sin \theta + \frac{\Gamma}{2\pi a}$$

$$\Rightarrow u^2 = u_\theta^2 = \cancel{4u^2 \sin^2 \theta} \quad 4u^2 \sin^2 \theta - \frac{2u\Gamma \sin \theta}{\pi a} + \frac{\Gamma^2}{4\pi^2 a^2}$$

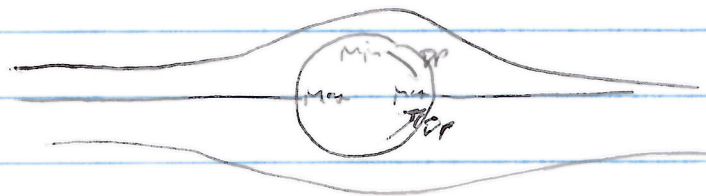
Bernoulli:

$$p + \frac{1}{2} \rho \left[ 4u^2 \sin^2 \theta - \frac{2u\Gamma \sin \theta}{\pi a} + \frac{\Gamma^2}{4\pi^2 a^2} \right] = \text{const}$$

↓  
constant  $\Rightarrow$  ignore

Note: (1) pressure is fore-aft symmetric  $\theta \rightarrow \pi - \theta$   
 so no drag force (d'Alembert's "paradox")

(2) pressure is a maximum at the stagnation points



Increasing pressure in direction of flow can lead to separation of boundary - see later in course.

If we take the y component of the pressure force on the cylinder

$$F_y = \int -p \sin\theta \underbrace{a d\theta}_{\text{area}}$$

$$= \rho \int \left[ 2u^2 \sin^2\theta - \frac{u\Gamma}{\pi a} \sin\theta \right] \sin\theta d\theta$$

↑  
odd in  $\theta \rightarrow$  average is zero

$$\underline{\underline{-\rho u \Gamma}} \quad \text{since} \quad \int \sin^2\theta d\theta = \pi$$

This is a specific case of the much more general Kutta-Joukowski theorem

For irrotational, 2D flow around any ~~any~~ shaped body ~~the~~ the lift force is given by

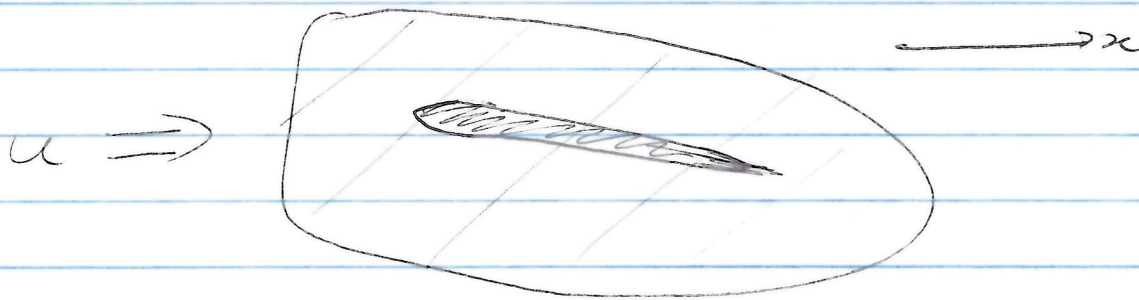
$$F_y = -\rho u \Gamma$$



8.4

Kutta-Joukowski lift formula

(Handout?)



Momentum flux

$$F_i = \oint \underbrace{(\rho S_{ij} + \rho v_i v_j)}_{\text{Momentum flux}} dS_j$$

perturbed  $x$  velocities  $\delta v_x = v_x - u$  $\rightarrow$  Bernoulli  $p \approx p_0 - \rho u \delta v_x$ 

Total mass flux must be zero

$$\oint \rho (v_x dS_x + v_y dS_y) = \oint \rho (\delta v_x dS_x + \delta v_y dS_y) = 0$$

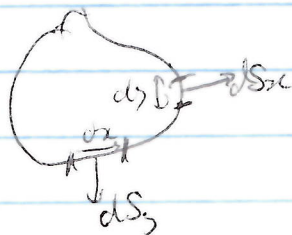
Taking the  $y$  component of  $F$ :

$$F_y = - \oint \rho v_y v_x dS_x + \underbrace{(p + \rho v_y v_y)}_{\text{ignore}} dS_y$$

$$= - \oint \rho \underbrace{v_y v_x}_{u \delta v_y - \text{cancel}} dS_x + \underbrace{(p_0 - \rho u \delta v_x + \rho v_y v_y)}_{\text{ignore}} dS_y$$

$$\approx - \oint p_0 dS_y - \rho u \oint (\delta v_y dS_x - \delta v_x dS_y)$$

In 2D



$dS_x = dx$

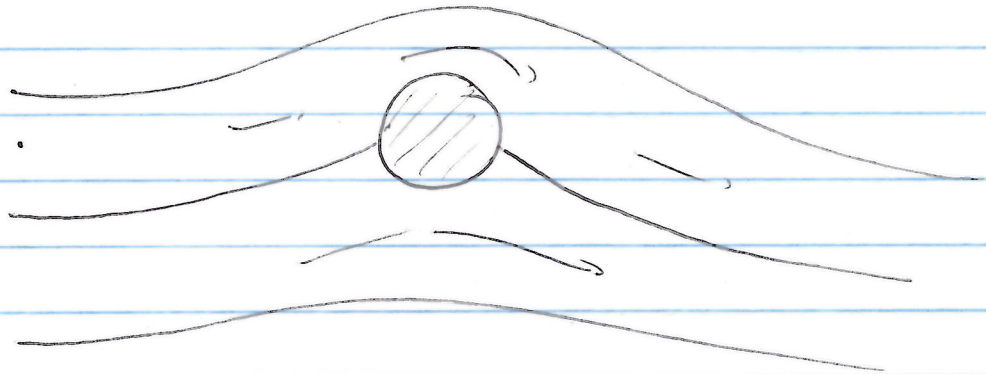
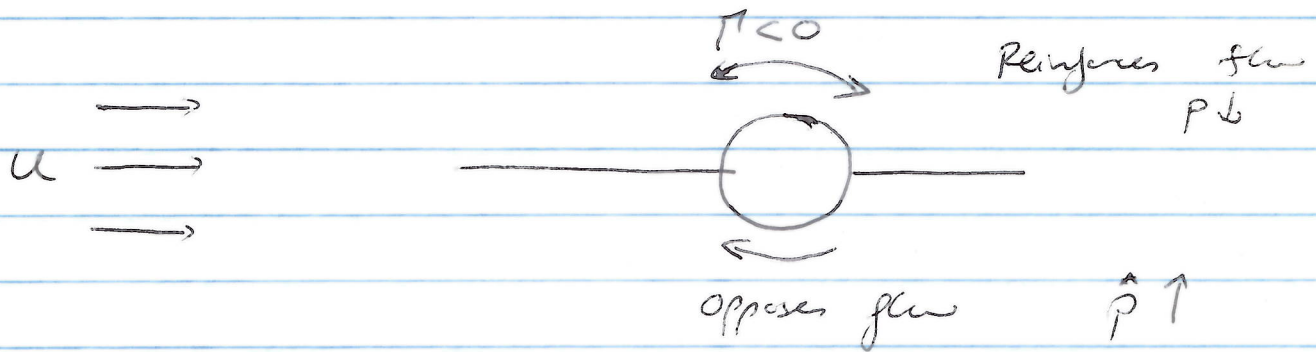
$dS_y = -dy$

$$\Rightarrow F_y = -\rho u \oint (\delta v_y dx + \delta v_x dy)$$



8.5

What does circulation do to the flow



Downwards flow of momentum  
 $\Rightarrow$  upwards push on body

What can cause  $\Gamma \neq 0$ ?

1. Rotation of body, friction and separation of boundary (not irrotational!)  
 $\rightarrow$  Magnus effect
2. Asymmetric shape w.r.t. oncoming flow  
 $\rightarrow$  Aerofoils!

